

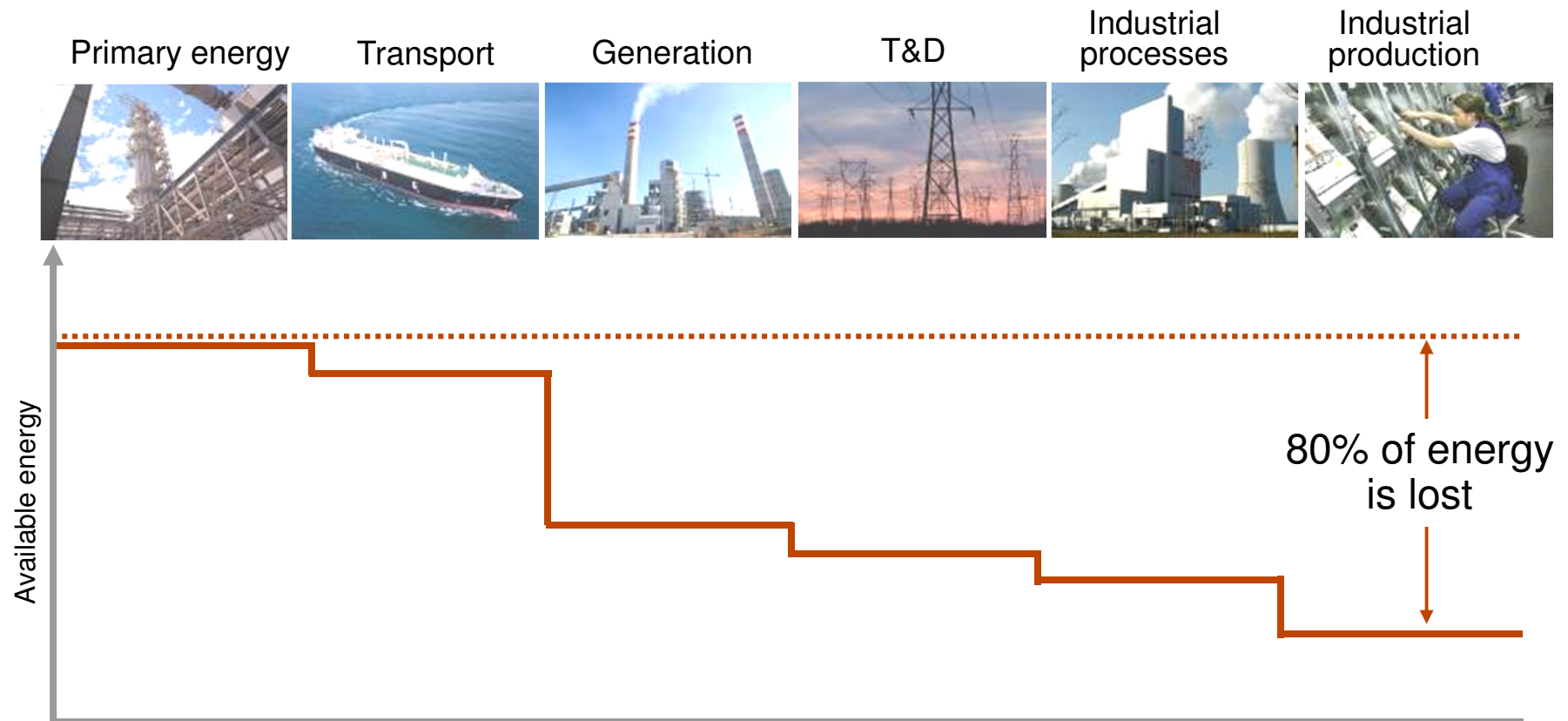
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# Solutions for Performance Monitoring, Diagnosis and Optimization of Power Plants

# Agenda

- Introduction
- Carbon-in-Ash Instrument
- Mill Runback Calculator.
- Combustion Optimization
- Soot Blowing Optimization.
- Startup Optimization
- Life-time Calculation
- Temperature State Space Control
- Life Steam Flow Calculation
- Unit Control
- Energy Optimizer
- Process Quality Monitoring
- Loop Performance Monitoring
- Energy Efficiency Consulting

Only 20% of primary energy generates economic value  
The rest is lost to conversion processes, transportation  
and operational inefficiencies



# Motivation for optimization

## **Benefits**

- Reduce fuel consumption and emissions
- Increase flexibility
- Identify and rectify equipment problems
- Improve predictive maintenance and availability
- Optimize asset lifecycles

## **Measures**

- Tune control loops
- Optimize the combustion process and improve boiler controls
- Optimize ramp rates, low load running and startups
- Optimize operation of multiple generating units
- Monitor and predict plant performance
- Issue early warnings for equipment diagnosis and preventive maintenance

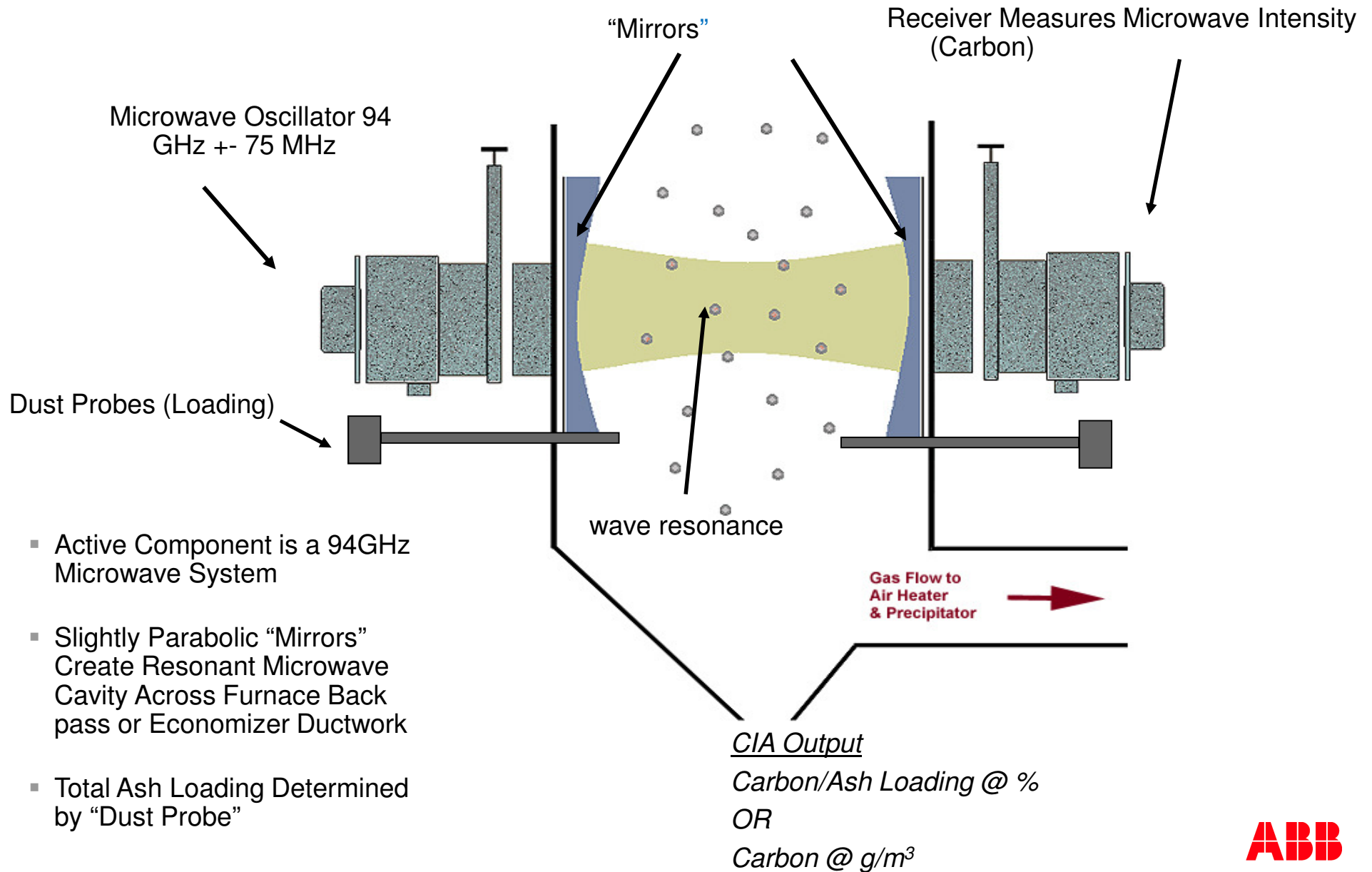
# Carbon In Ash Instrument Basics



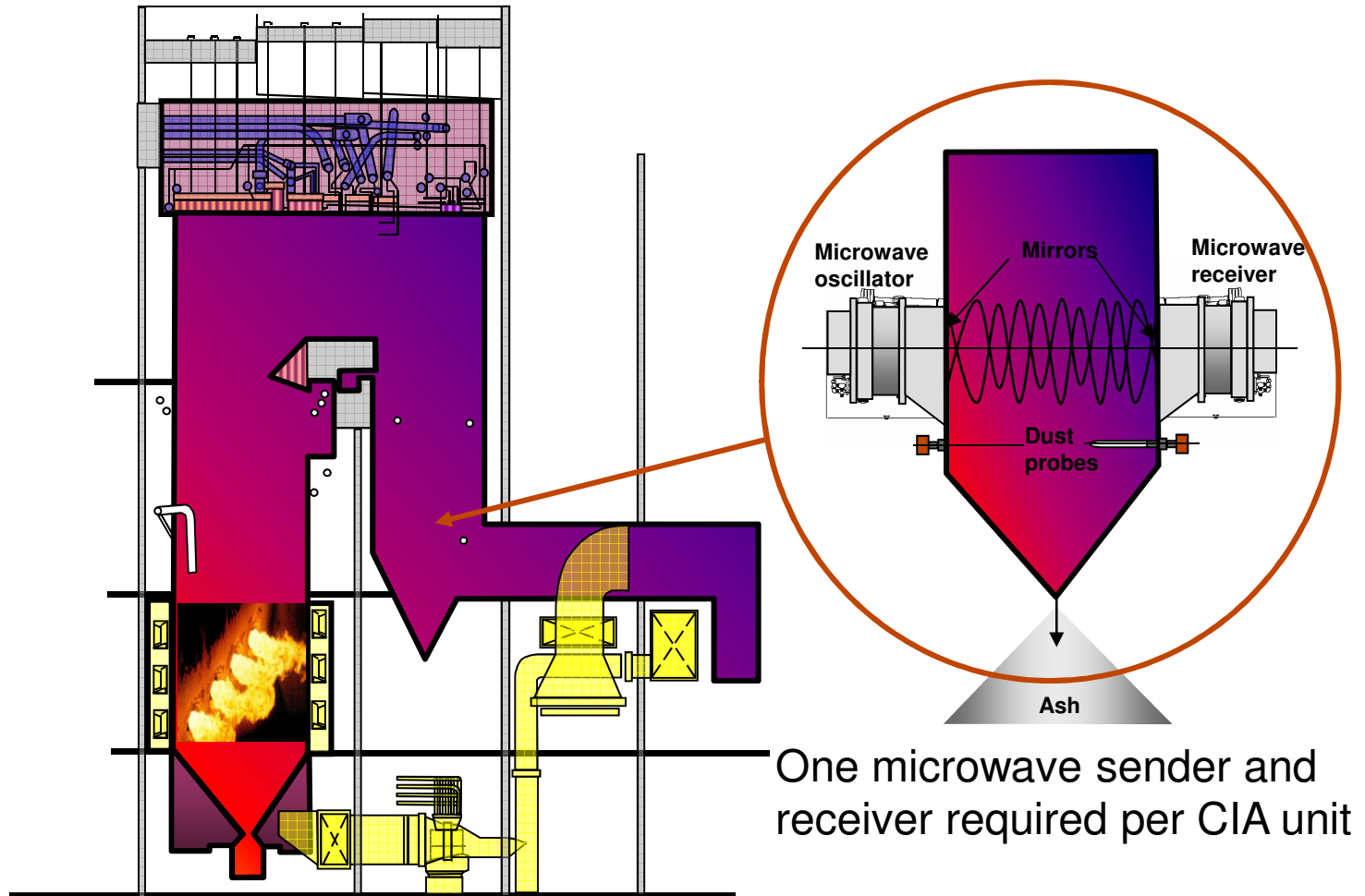
- Majority of the combustible portion of the ash accounting for the energy loss is simply unburned carbon.
- Unburned carbon is a highly variable parameter which is dependent upon coal type, load, fuel and air distribution, and other boiler-specific factors, the need for on-line real-time measurement has become more critical in combustion optimization process
- ABB Carbon In Ash Instrument (CIA) provides a true real-time and representative measurements of the unburned carbon in the fly ash for utility power plants

# Carbon In Ash Instrument

## ABB's Technology Edge!

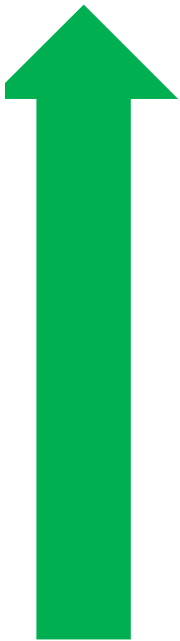


# Carbon In Ash Instrument Installation



# Carbon In Ash Instrument Benefits

Increased

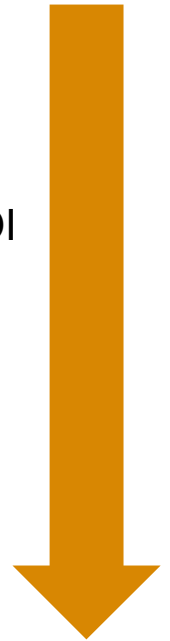


- Increased combustion efficiency
- Increased quality of Fly Ash resulting in better sale price!
- Improved Mercury capture
- Loss of Ignition availability
- Balanced plant efficiency



ABB's Carbon in Ash Instrument

- Reduced operating cost
- Reduced amount of Fly Ash & reduced Land Filling
- Reduced manual LOI procedure

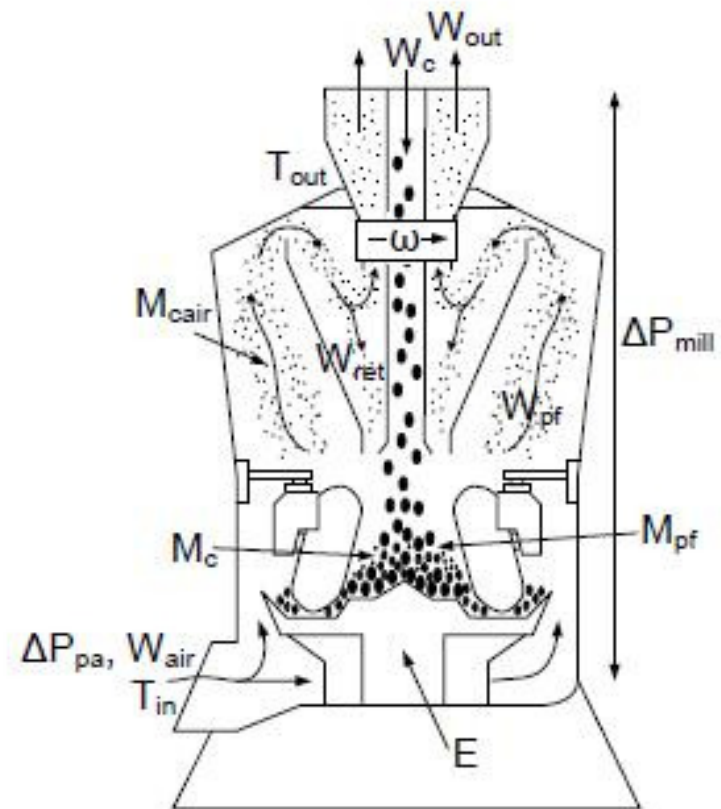


Reduced



# OPTIMAX<sup>®</sup> Performance Mill Run Back Calculator

- Run-Back Calculator based on physical model of the mill
- Outputs:
  - Maximal Drying capacity
  - Maximal grinding capacity
  - Moisture of coal / biomass
- Implemented on controller

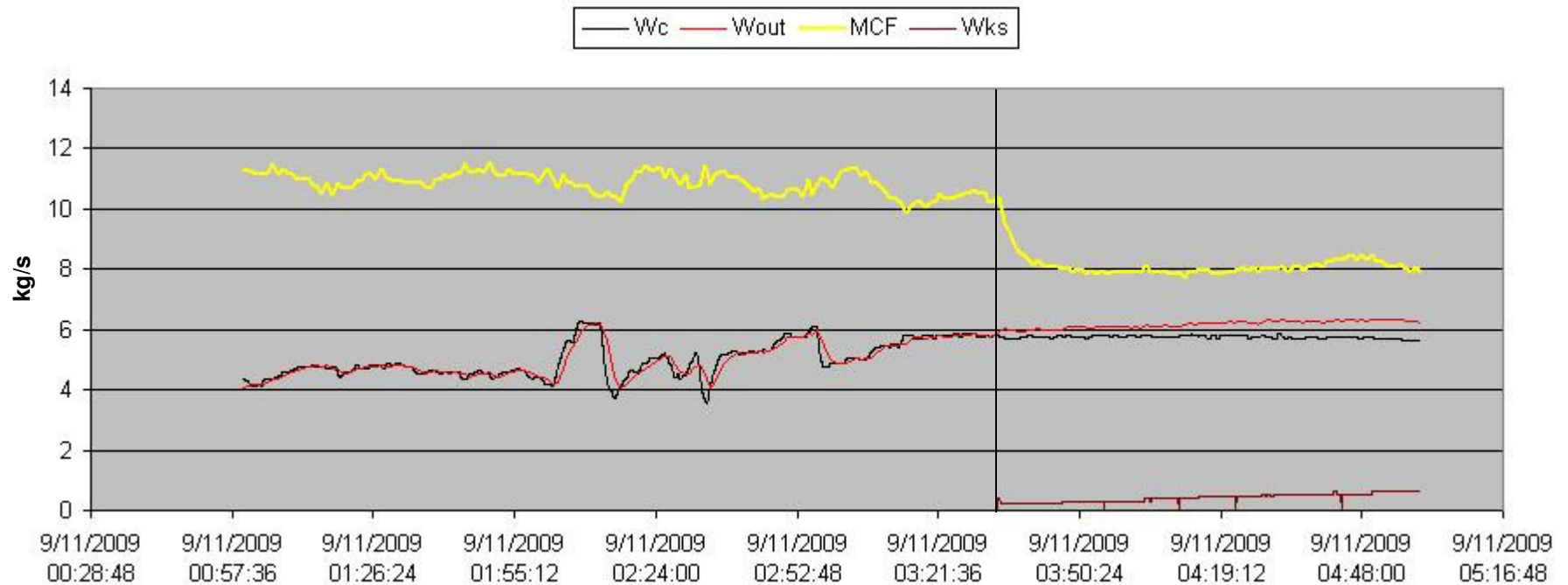


Referenz:

P. Niemczyk et al: Derivation and validation of a coal mill model for control

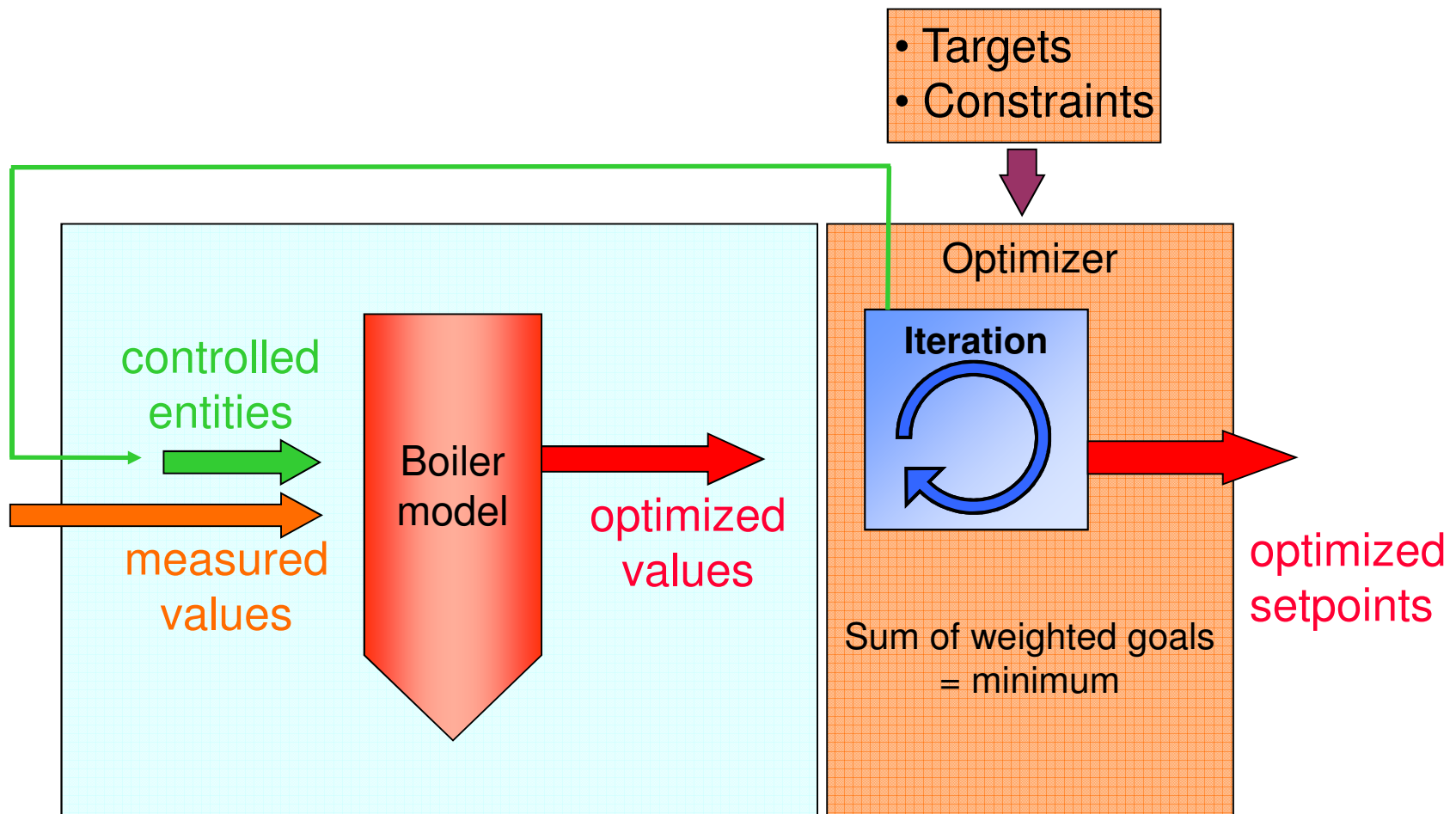
# OPTIMAX® Performance

## Mill Drying capacity



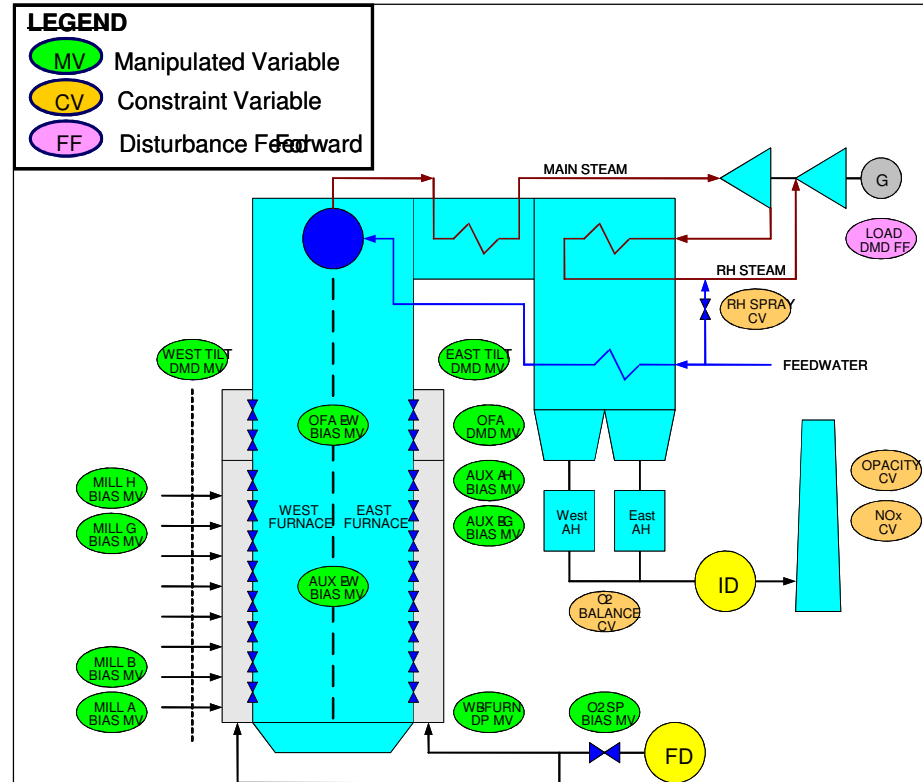
- MCF: Max. coal/biomass addition
- 3:30: Addition of Biomass

# Combustion Optimization Principle



# Combustion Optimizer Typical Scope

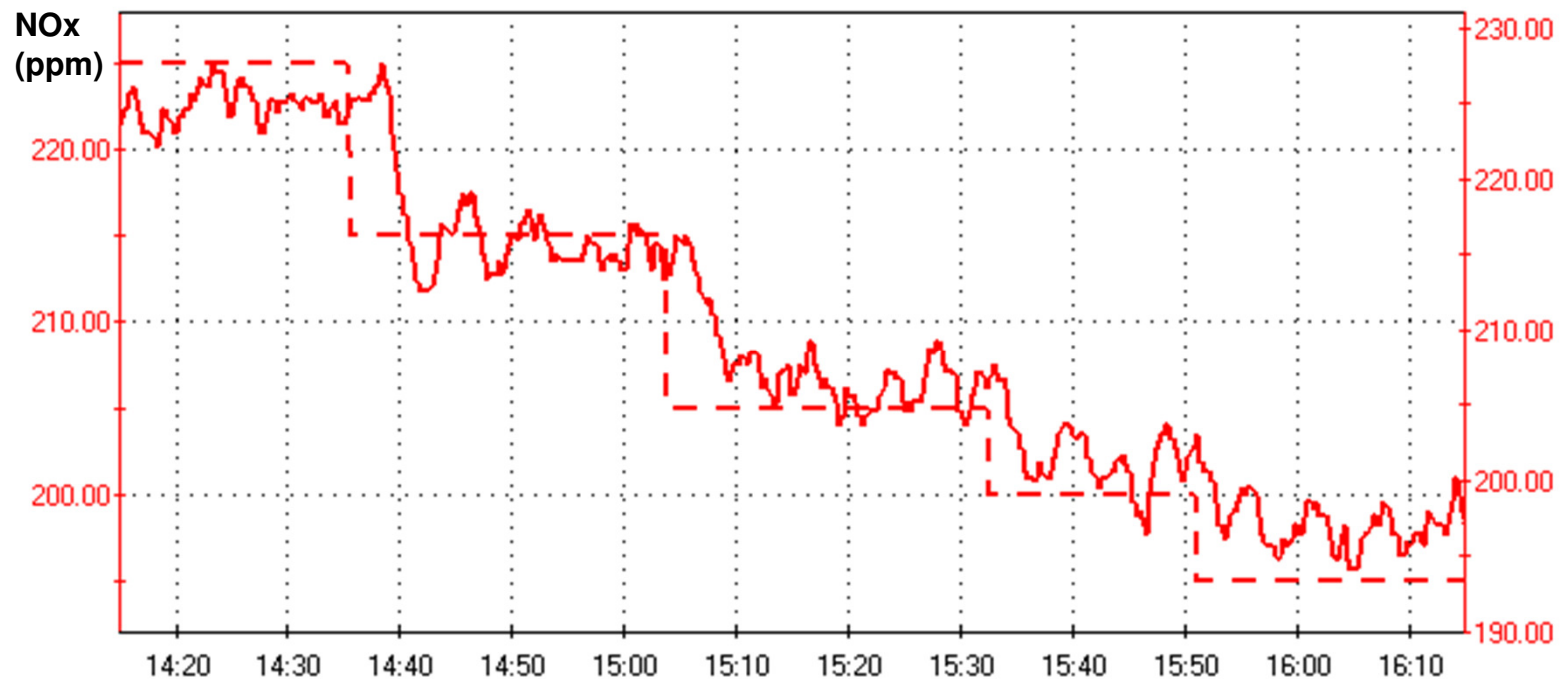
- NOx – maximum constraint, main objective
- Opacity – maximum constraint, noisy value
- O2 imbalance – delta O2 between furnaces, controlled with furnace biases on Aux Air and OFAD
- Actuator constraints – must keep base DCS loops in operating range, usually below a max output
  - Spray valves
  - Dampers



# Combustion Optimizer

## Reference: reducing NOx

- Max limit lowered sequentially by 10 ppm from 225 to 195



# Lifetime Monitoring Motivation

## Boilers

- Increasing peak operation results in additional load cycles on individual components
- New component materials allow higher steam parameters
- Optimum plant or boiler operation is achieved when the:
  - Operation is safe, and when there is
  - Good Agreement between design and the current operating lifetime consumption

## Turbines

- Requirement for operational safety and high availability
- Obligation to prevent highly stressed components from failing,
  - due to:
    - Permanent loads such as high pressures and temperatures
    - Centrifugal forces in a high temperature range
    - Low-frequency alternating loads

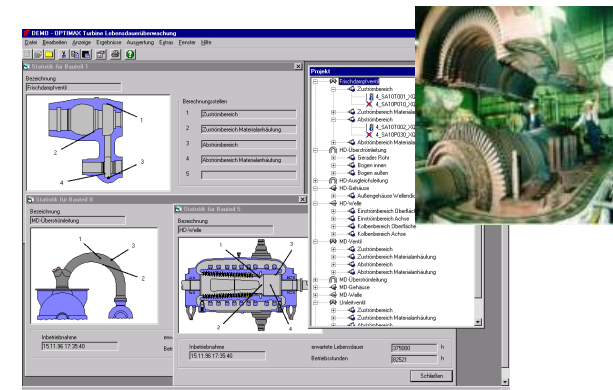
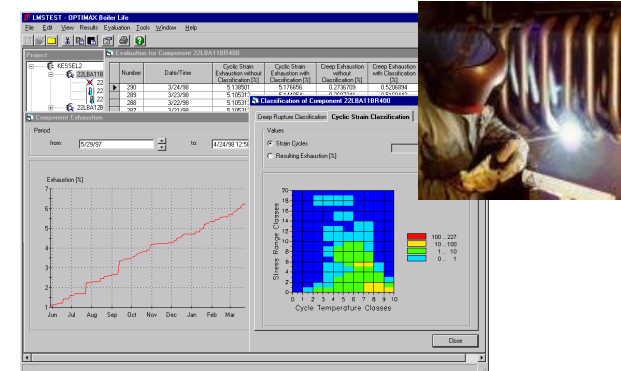
# Lifetime Monitoring Boiler and Turbine

## Features

- Online calculation of lifetime consumption of critical components
- BoilerLife certified by TÜV
- Calculations according to international standards
- Online reporting on lifetime status of critical components

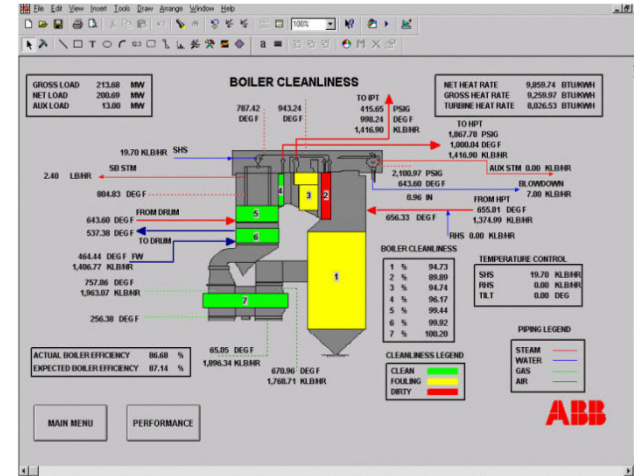
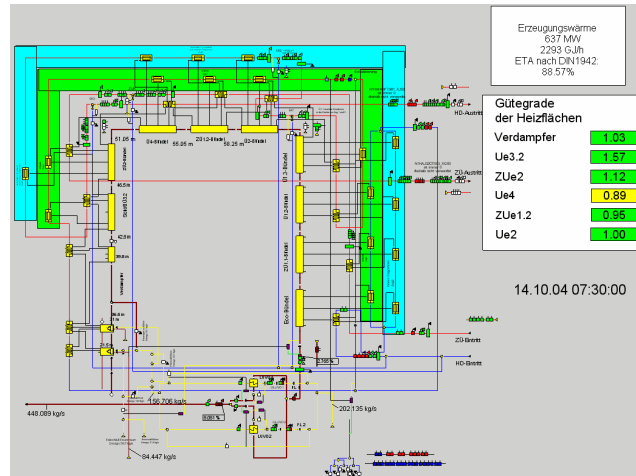
## Benefits

- Improving maintenance planning
- Ensure that components will not fail or need replacement too early
- Certified reporting to safety authorities



# Soot Blowing Optimization

## Model based calculation of heat exchangers



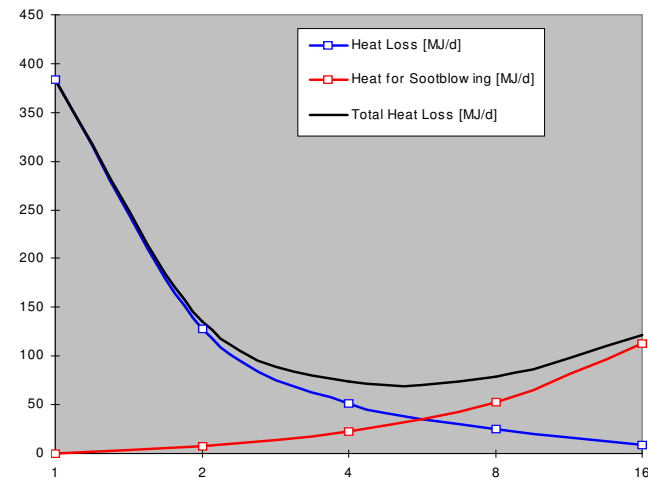
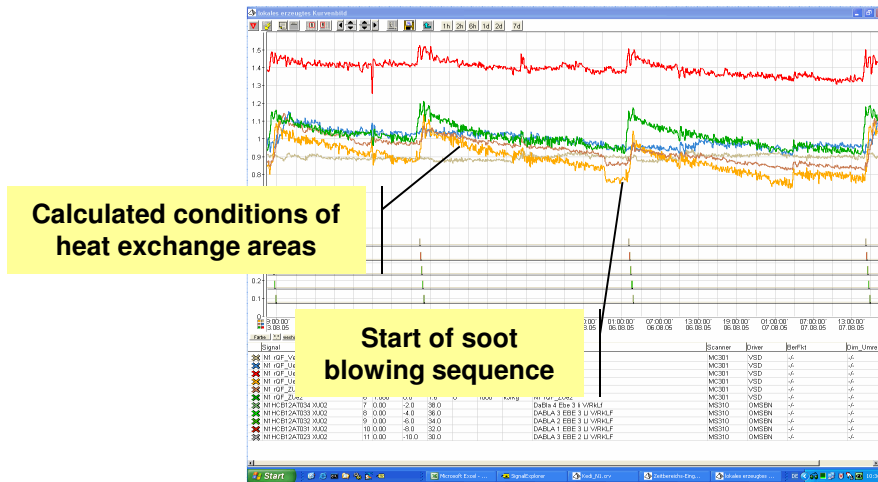
Activation signals for individual soot blower groups are:

- Temperature limits
- Soot blower steam consumption
- Water consumption of water injectors
- Boiler efficiency
- Injection rates of intermediate superheaters
- Pressure losses
- Blower performance



# Soot Blowing Optimization

## Calculation results with a detailed boiler model



### Features

- Provides operator guidance as to when to initiate a soot blowing sequence
- Calculates cleanliness factors per section
- Measures heat transfer efficiency
- Applies to furnace, walls and convective sections

### Benefits

- Easy-to-spot effects of minor changes in soot blowing sequences
- Significant heat rate savings
- Increase in long term plant performance
- Online computation of surface cleanliness
- Typical payback time < 2 years

# BoilerMax

## Boiler start-up Optimization

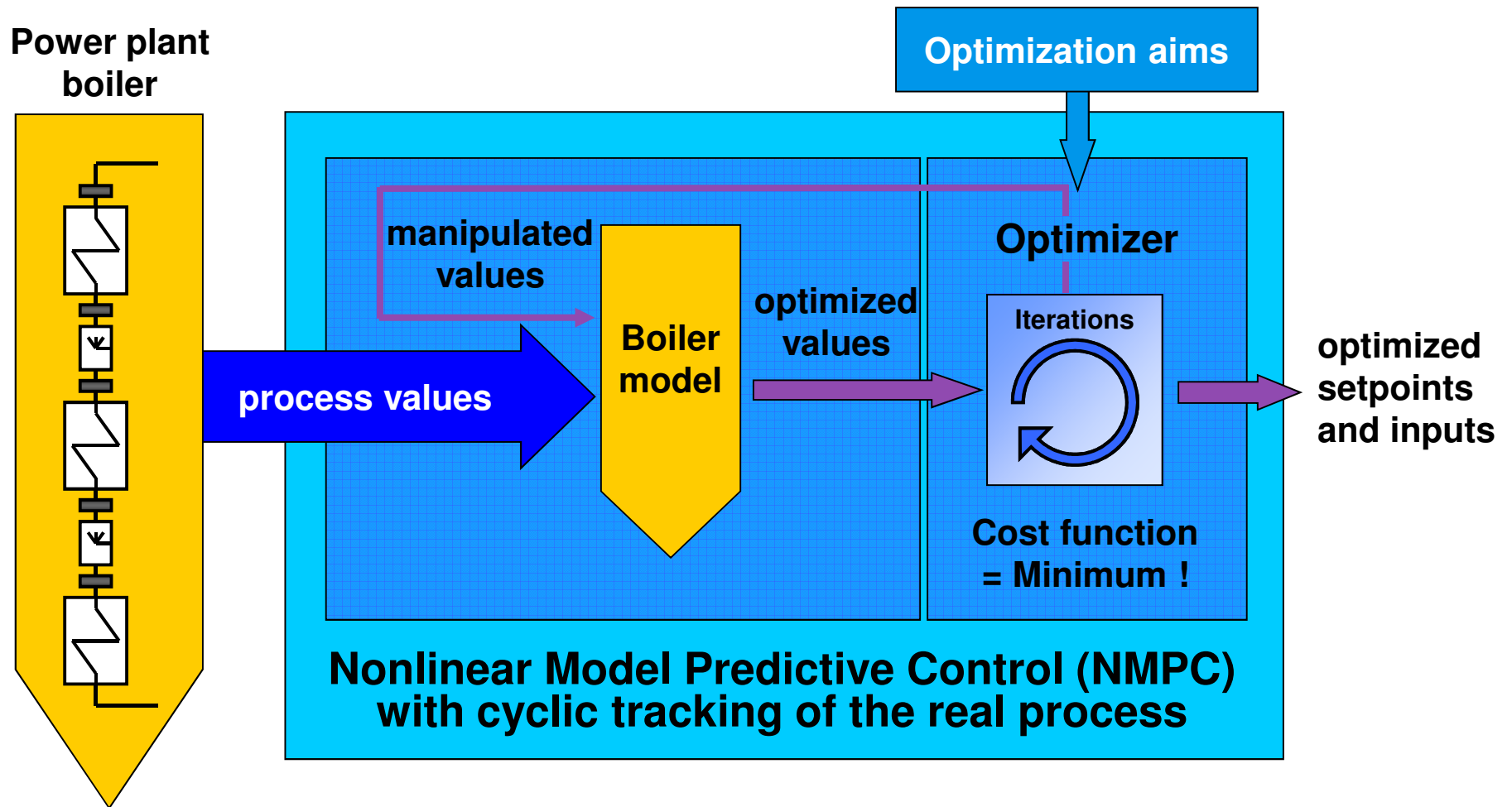


### Benefits:

- Shorter start-up and shut-down time reduces fuel consumption
- Faster load response to load dispatcher, advantages in energy trading
- Explicit consideration of thermal stresses in thick-walled components, control of temperature variances during start-up
- Earlier warm-up and speed-up of the steam turbine and therefore earlier grid synchronization possible

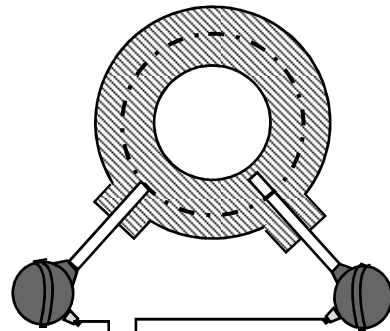
# BoilerMax

## Functional principle



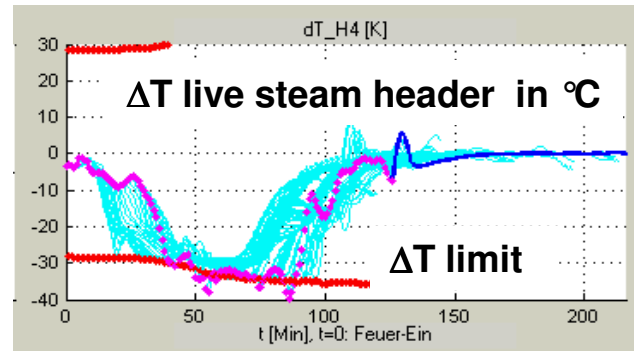
# BoilerMax

## Determination of thermal stresses



$T_i$ : inner temperature  
 $T_m$ : mid temperature

$$\Delta T \approx T_m - T_i$$



### Principle:

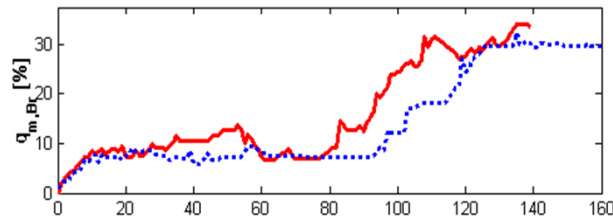
- Temperature difference  $\Delta T$  is indicator for thermal stresses
- Measurement of  $\Delta T$  between inner surface and the mean diameter of the annular cross section of thick-walled components
- Alternative 1: determination on non-heated surface
- Alternative 2: indirect determination from steam temperature gradients

# BoilerMax

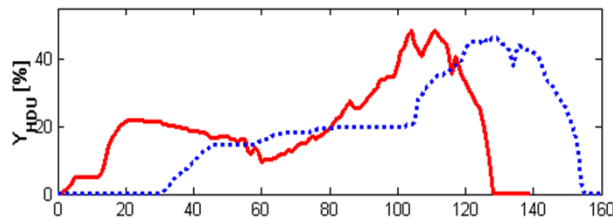
## Enhanced start-up phase

### Traditional – BoilerMax

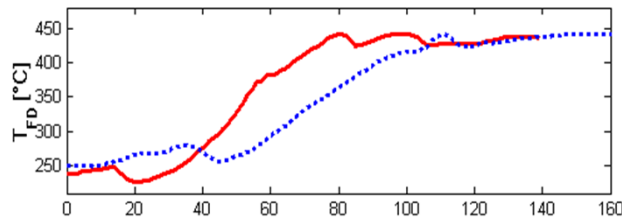
Fuel flow



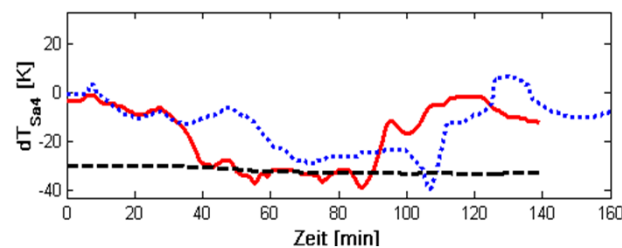
HP-Bypass position



LS temperature



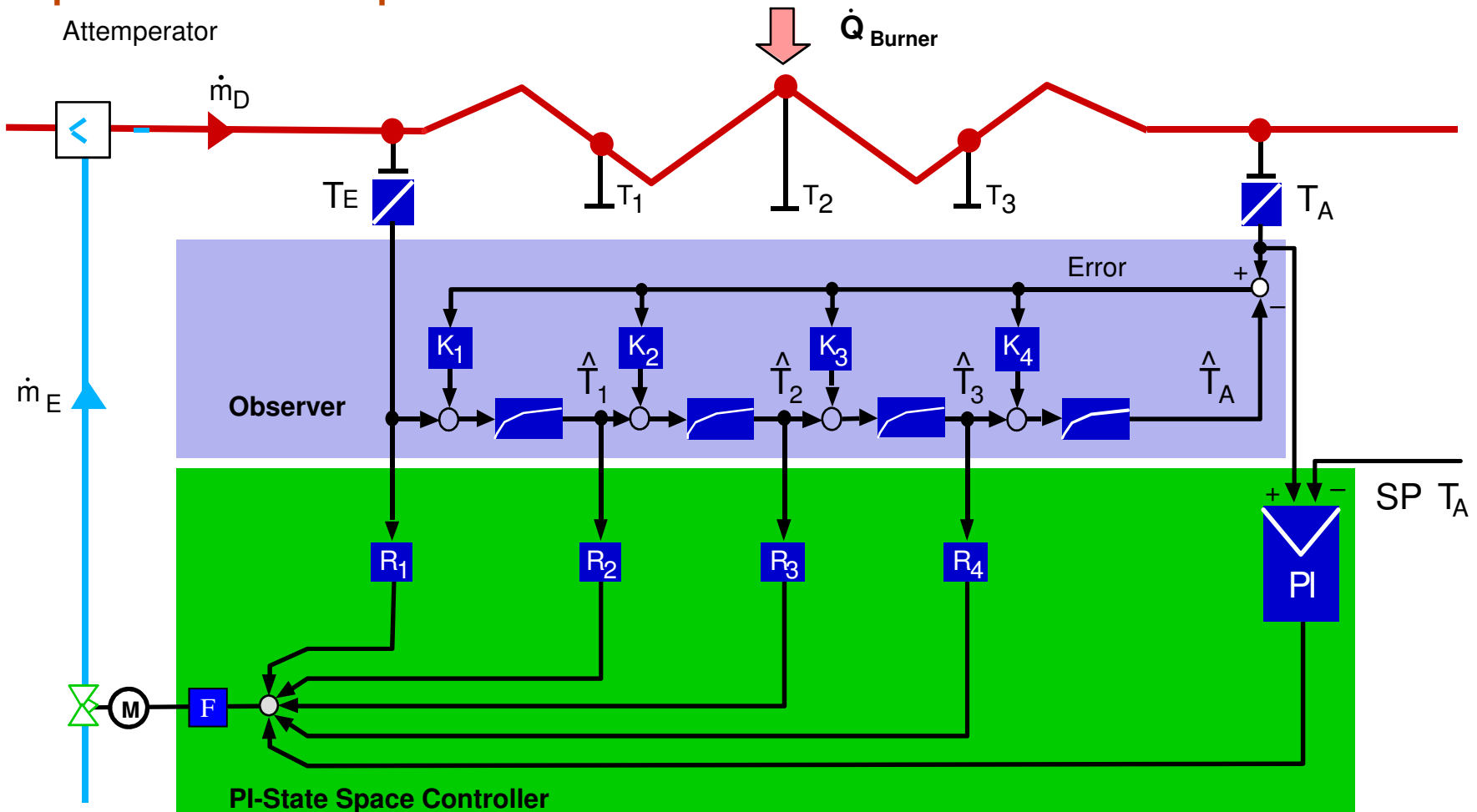
dT thick-walled component



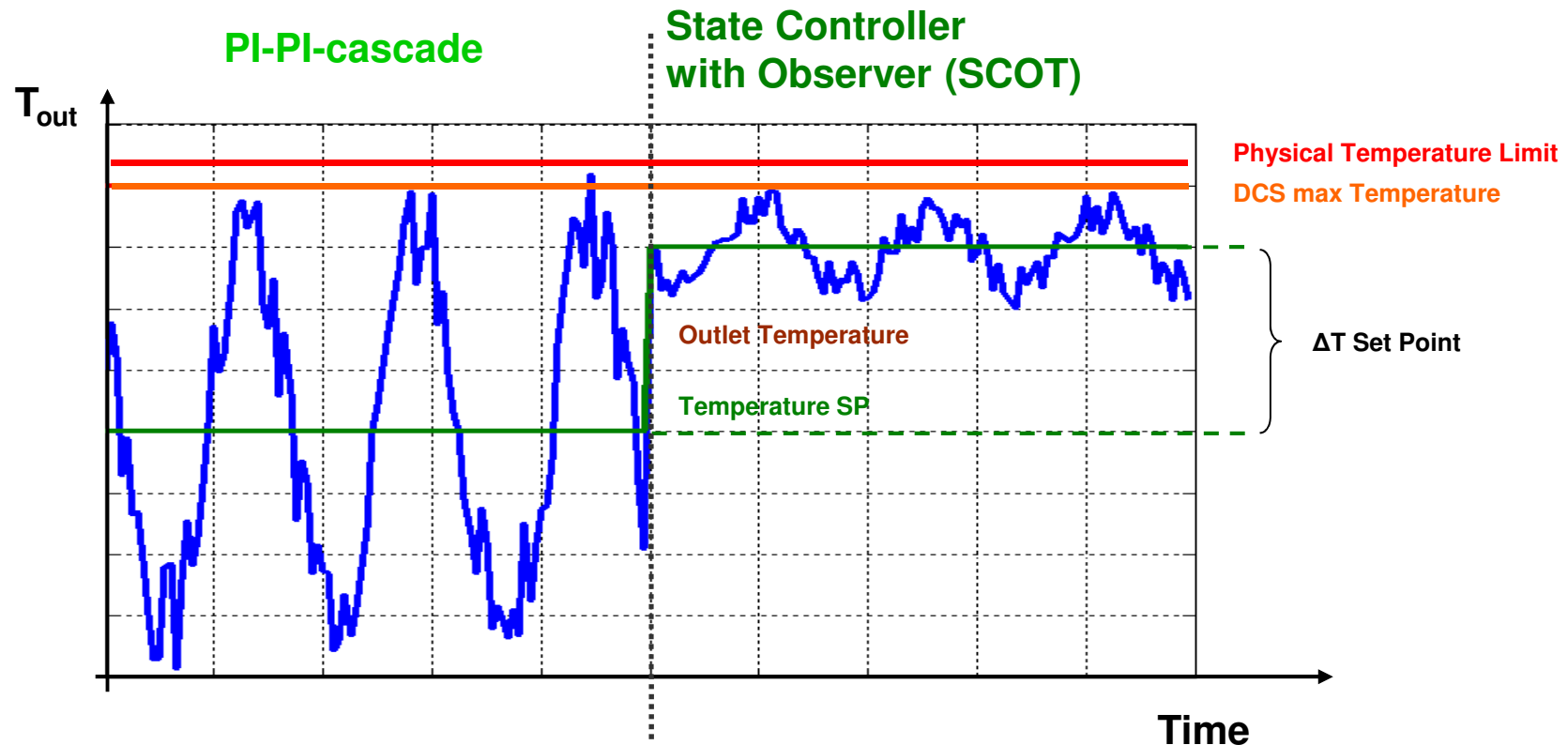
- Traditional start-up to comply with design limits
- BoilerMax start-up allows exploitation of design limits for more efficient process control:
  - Based on process model
  - NMPC technology
  - Predictive coordination of multiple variables
  - Online optimization in real-time

**Up to 15% savings due to fast and low-stress boiler start-up**

# State Space Controller Improved Temperature Control

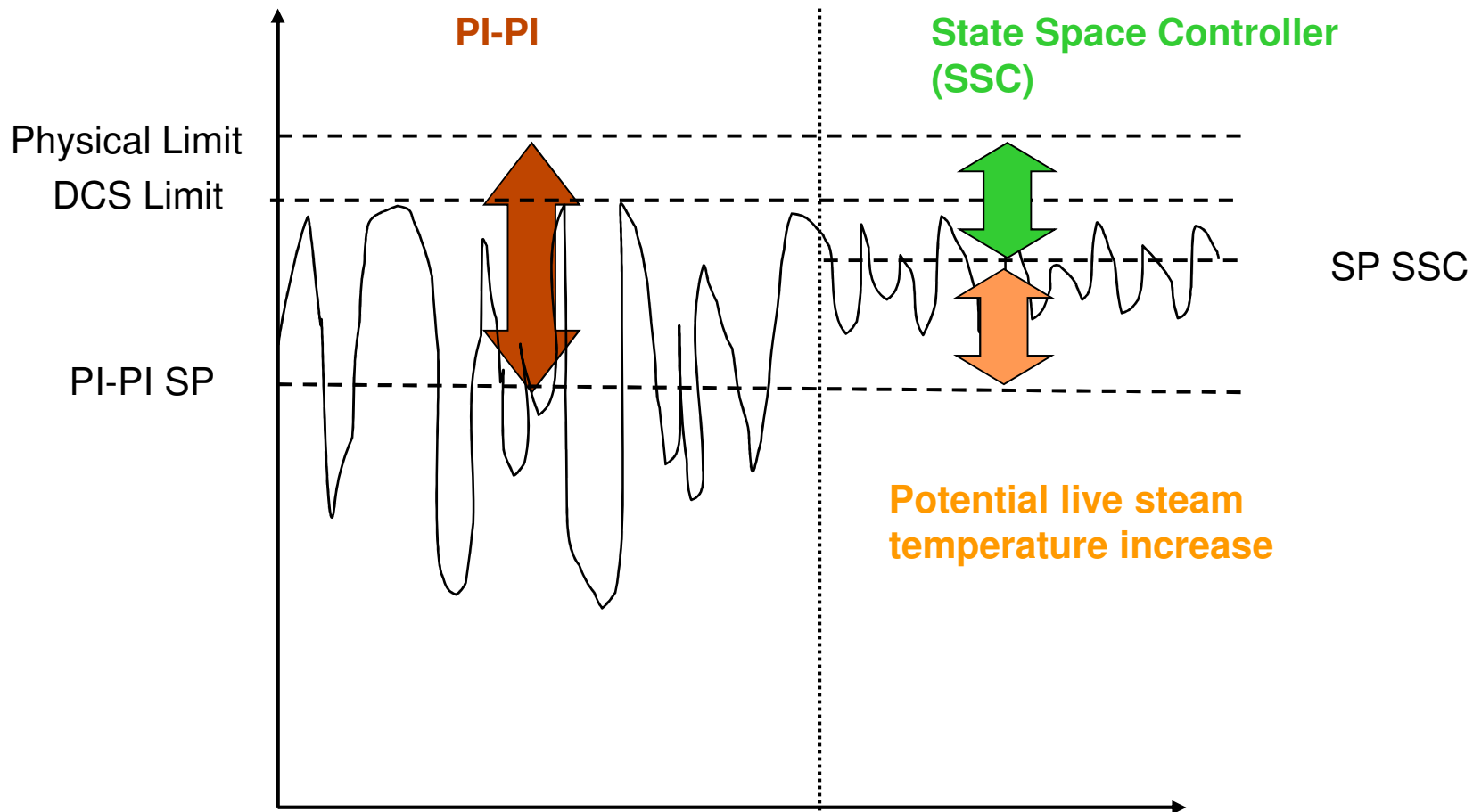


# State Space Controller Improved Temperature Control



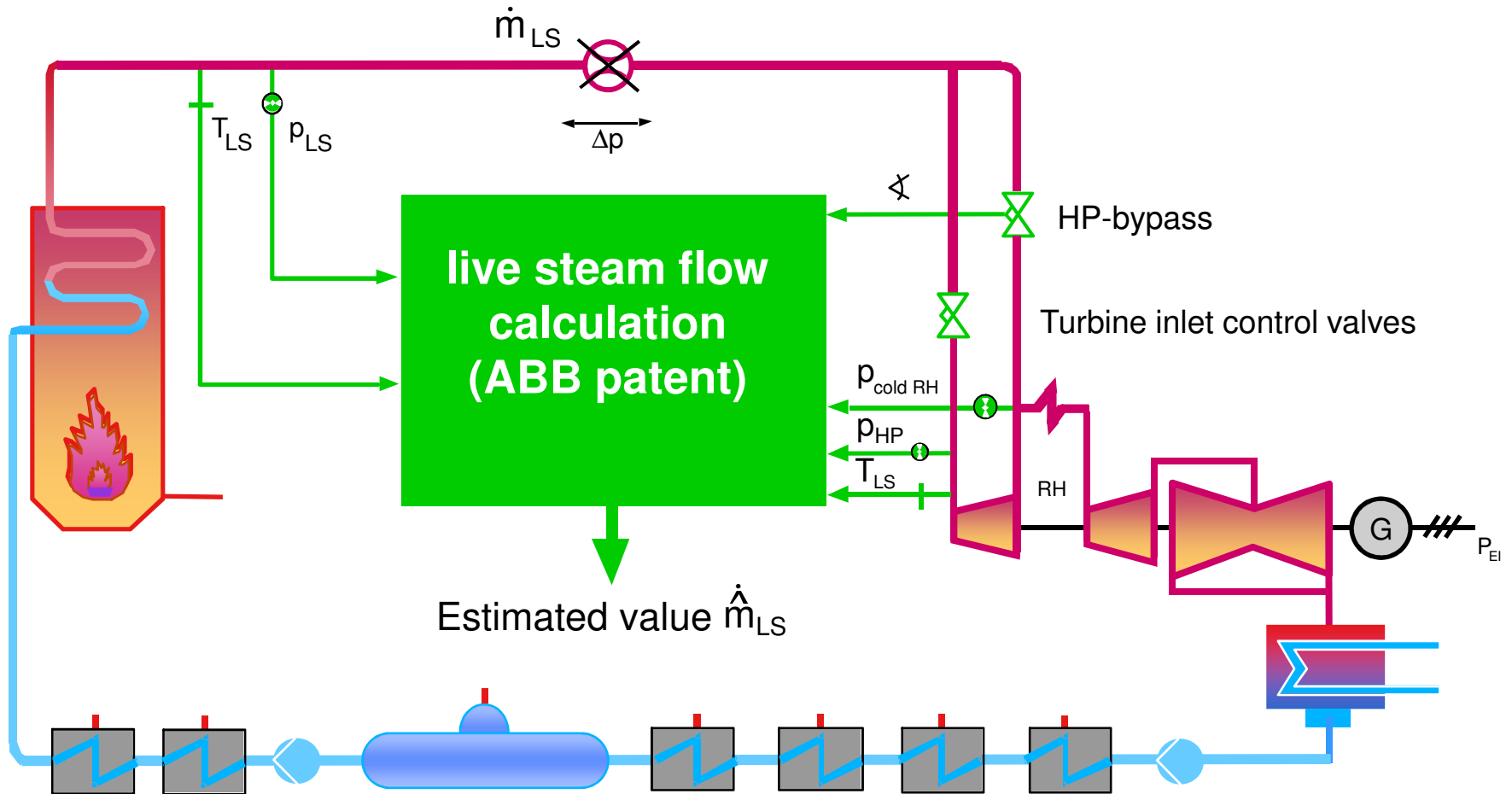
- Increasing the live steam and related steam operation temperature results in an immediate increment of unit efficiency
- With a higher set point, however, the margin between the operation point and max. admissible temperature is reduced
- This is no problem thanks to the improved performance that the state controller delivers

# OPTIMAX® State Space Controller Improved Temperature Control



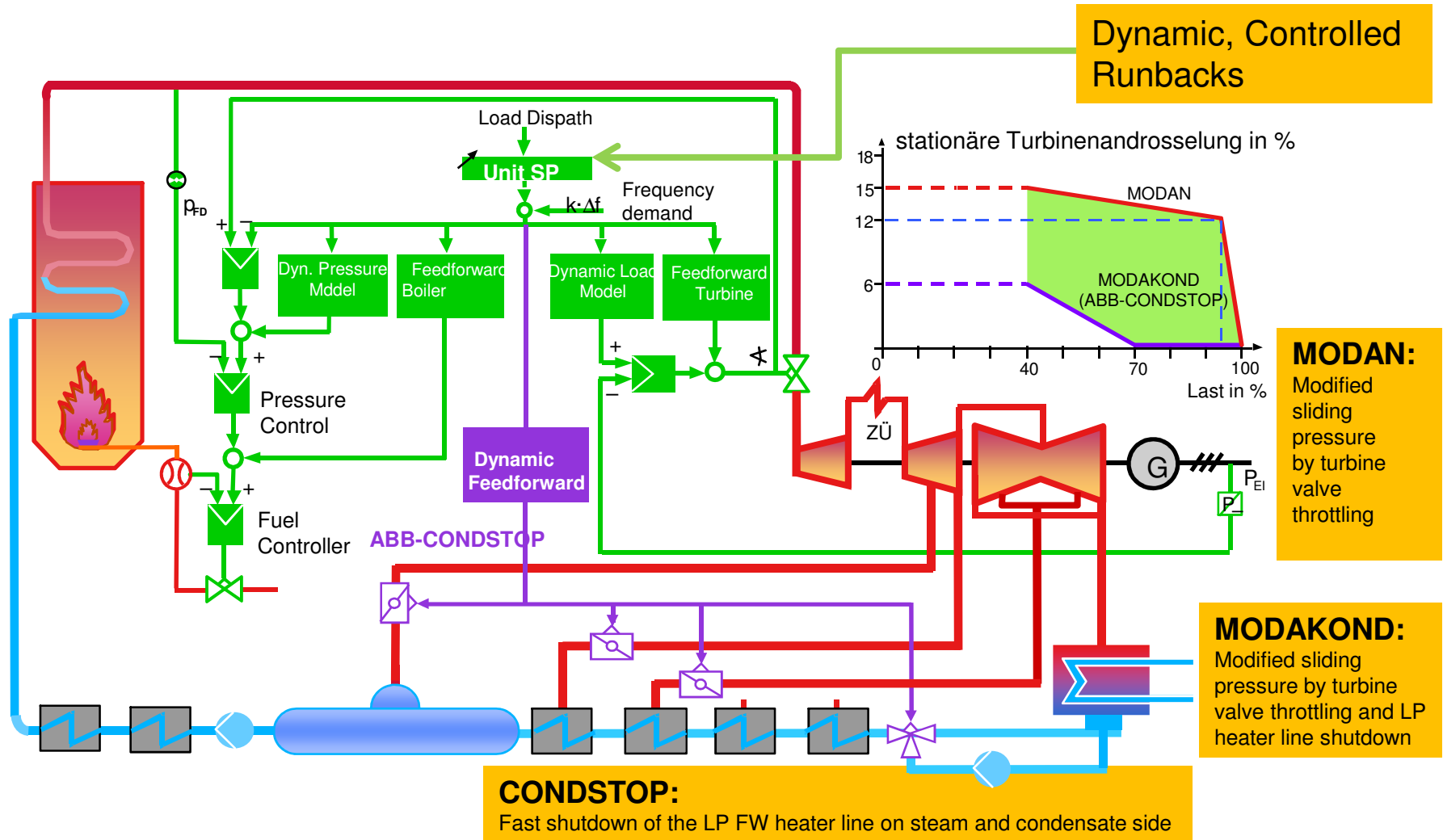


# Life Steam Flow Calculation Reduction of Throttling Losses



# Unit Control

## Flexible and Reliable Operation



# Energy Optimizer

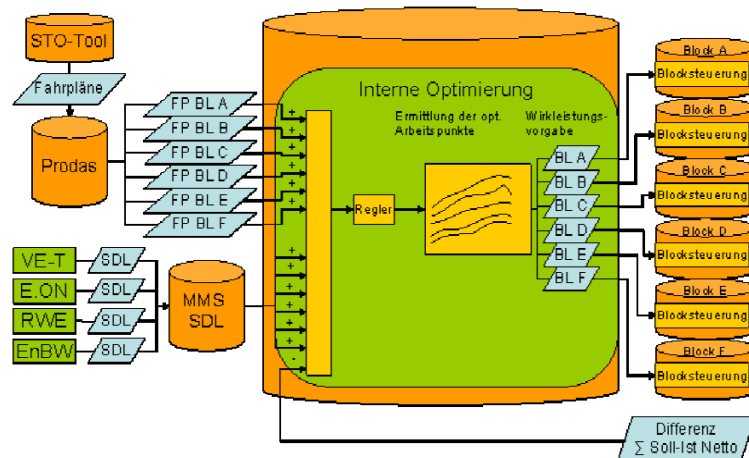


- Flexible exploitation of different production units
  - Gas turbines
  - Boilers
  - Steam turbines
  - Different fuels
- Varying operational policies.:
  - Prio steam production
  - Prio el. production
  - Start/Stop of boilers and turbines
- Energy Optimizer: Online-Optimization considering process constraints and market needs



# Reference 1: Internal Optimization Jänschwalde

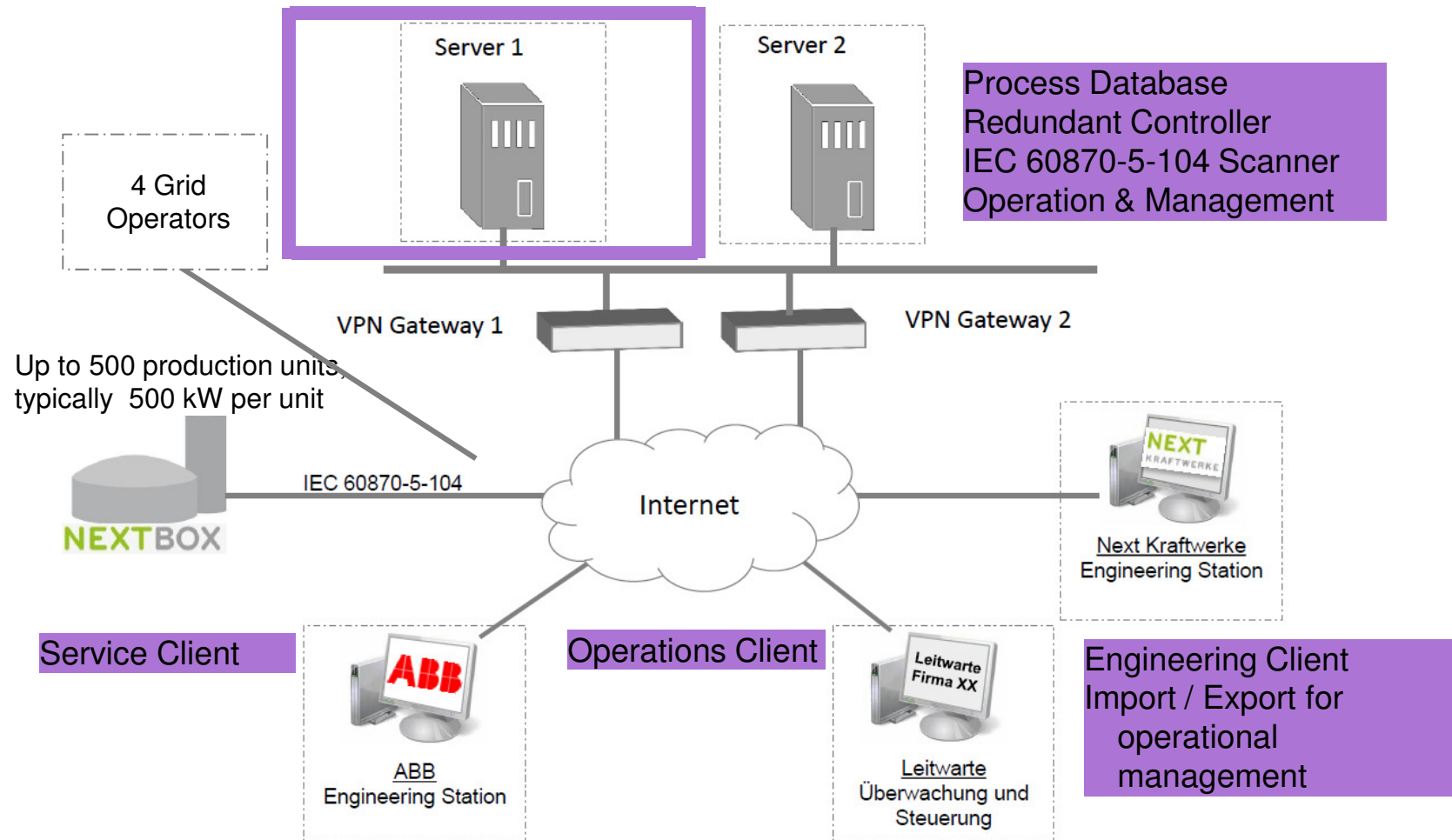
## Pooling of six 500 MW units



### Advantage of Multi-unit optimization

- Exploit communication network between management system and unit control system
- Real-time optimization of set points and secondary frequency control
- Fast and optimal reaction to fulfill production task, incl. gradients and timing of load ramps
- Goals:
  - minimize fuel consumption and CO<sub>2</sub>-emissions
  - increase flexibility

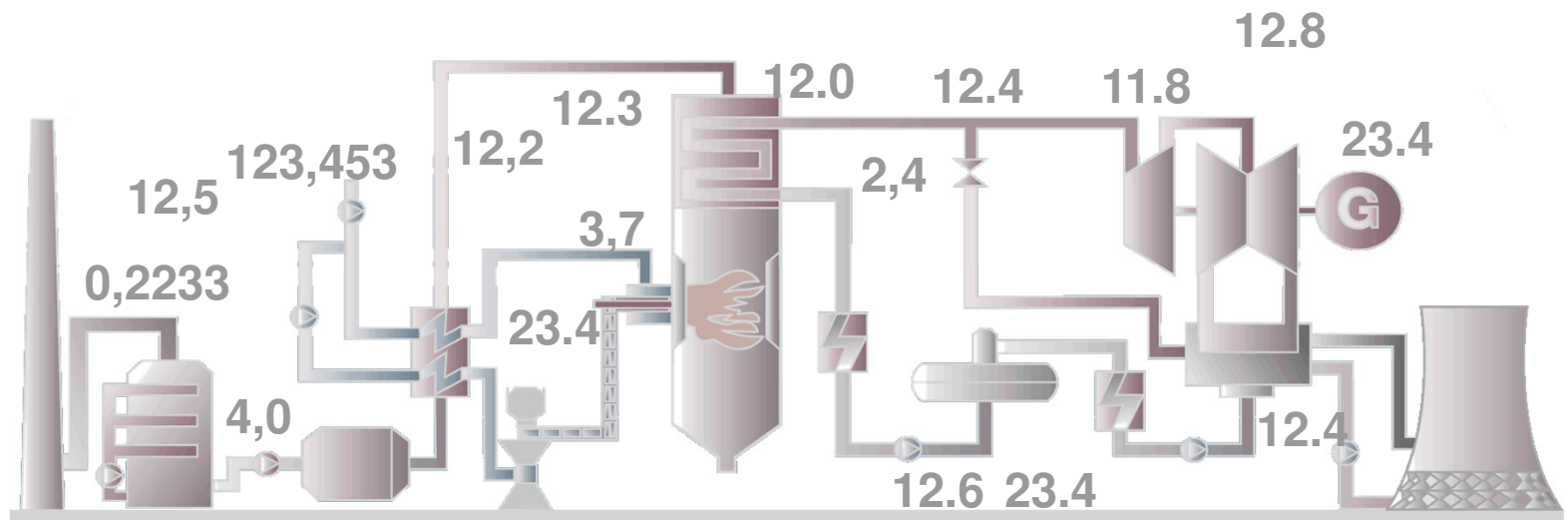
## Reference 2: Pooling of up to 500 biogas plants



# OPTIMAX® PlantPerformance

## Starting point: Monitoring of Process Values in DCS

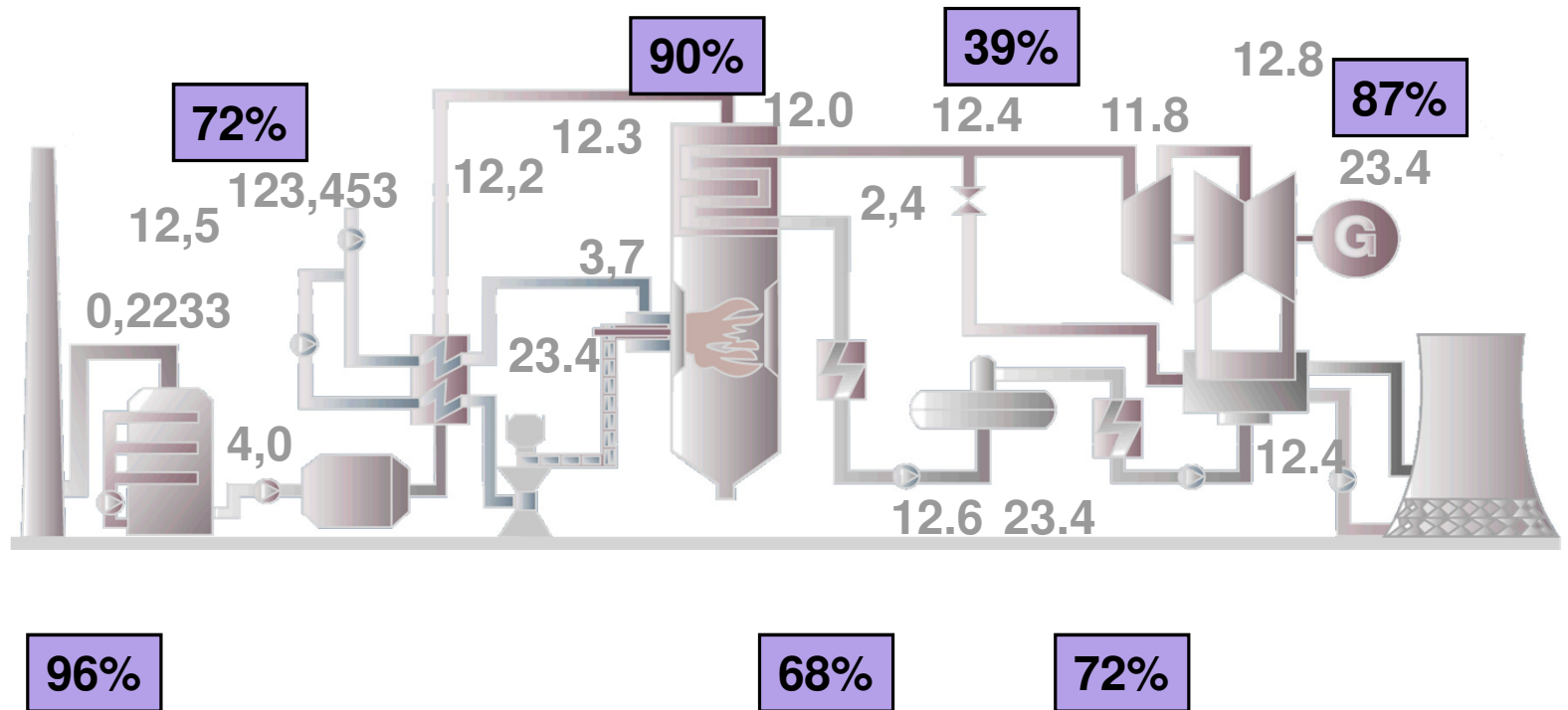
- Process values alone usually give no information about the efficiency or the process quality of a plant



# OPTIMAX® PlantPerformance

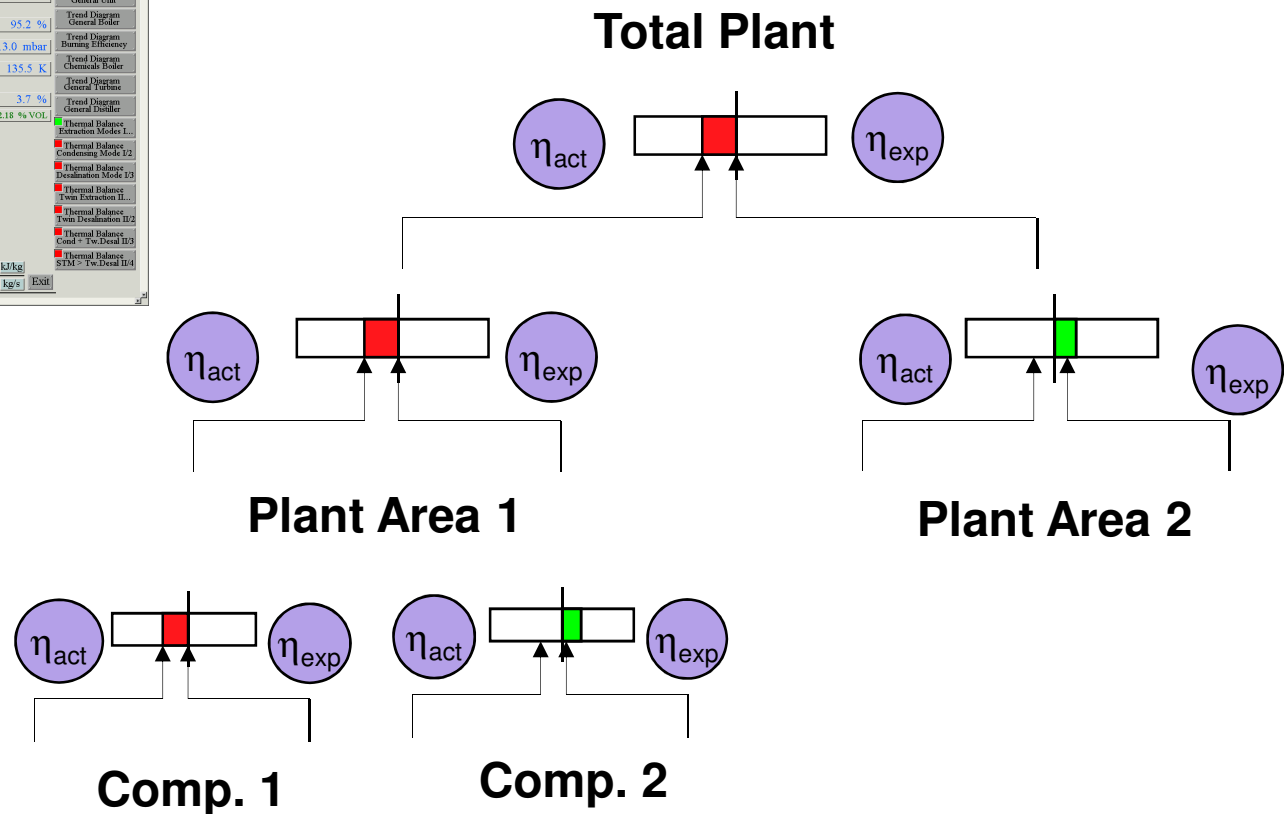
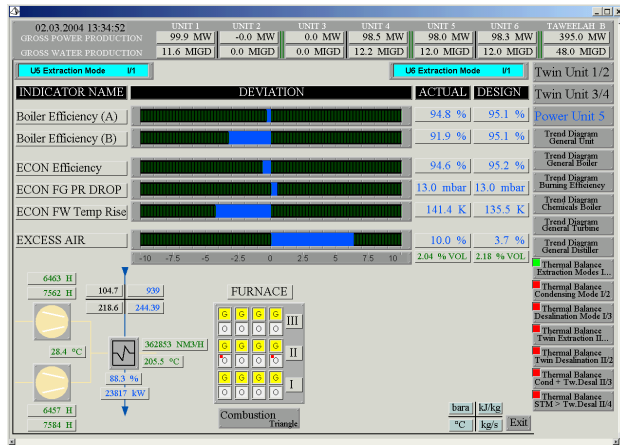
## Determination of Performance Indicators

- Performance indicators are determined by using multiple process values



# OPTIMAX® PlantPerformance

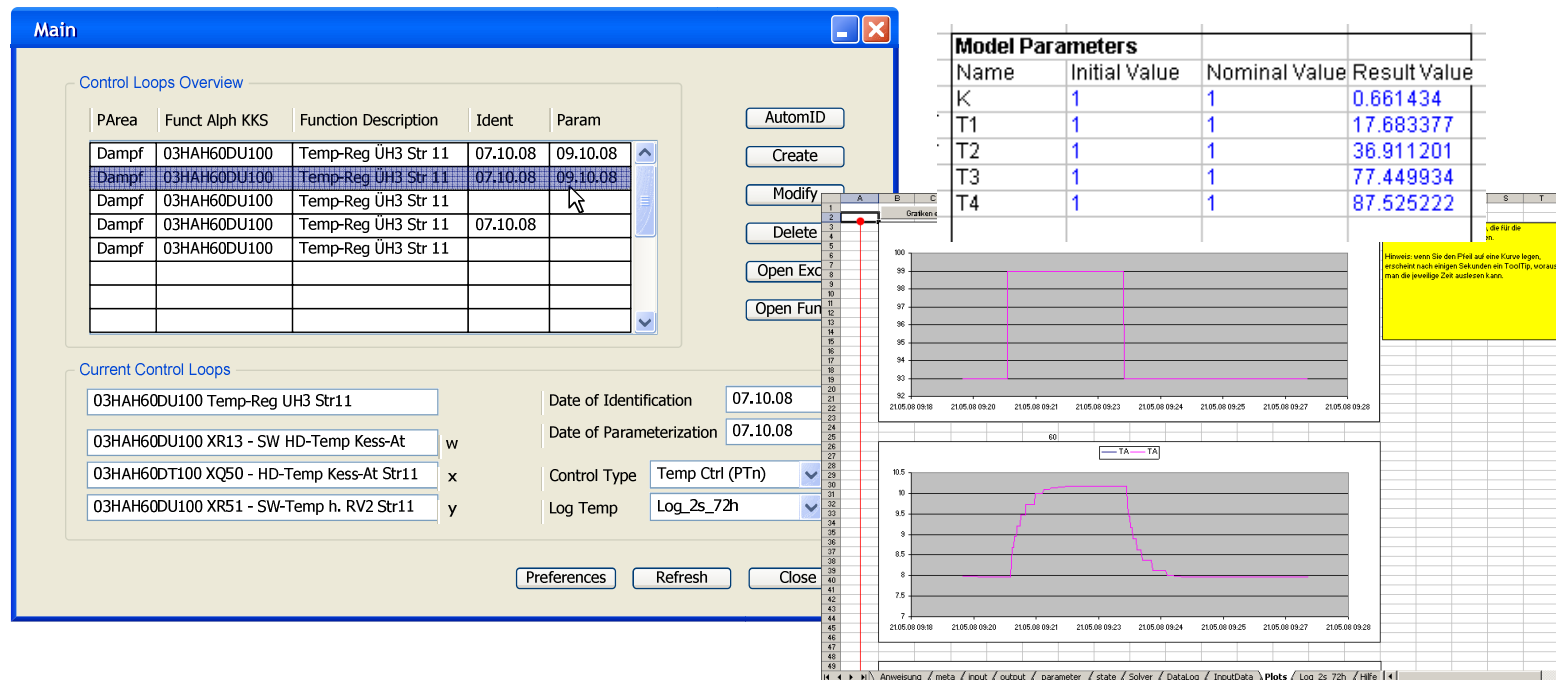
## Identifying the origin of a performance deviation





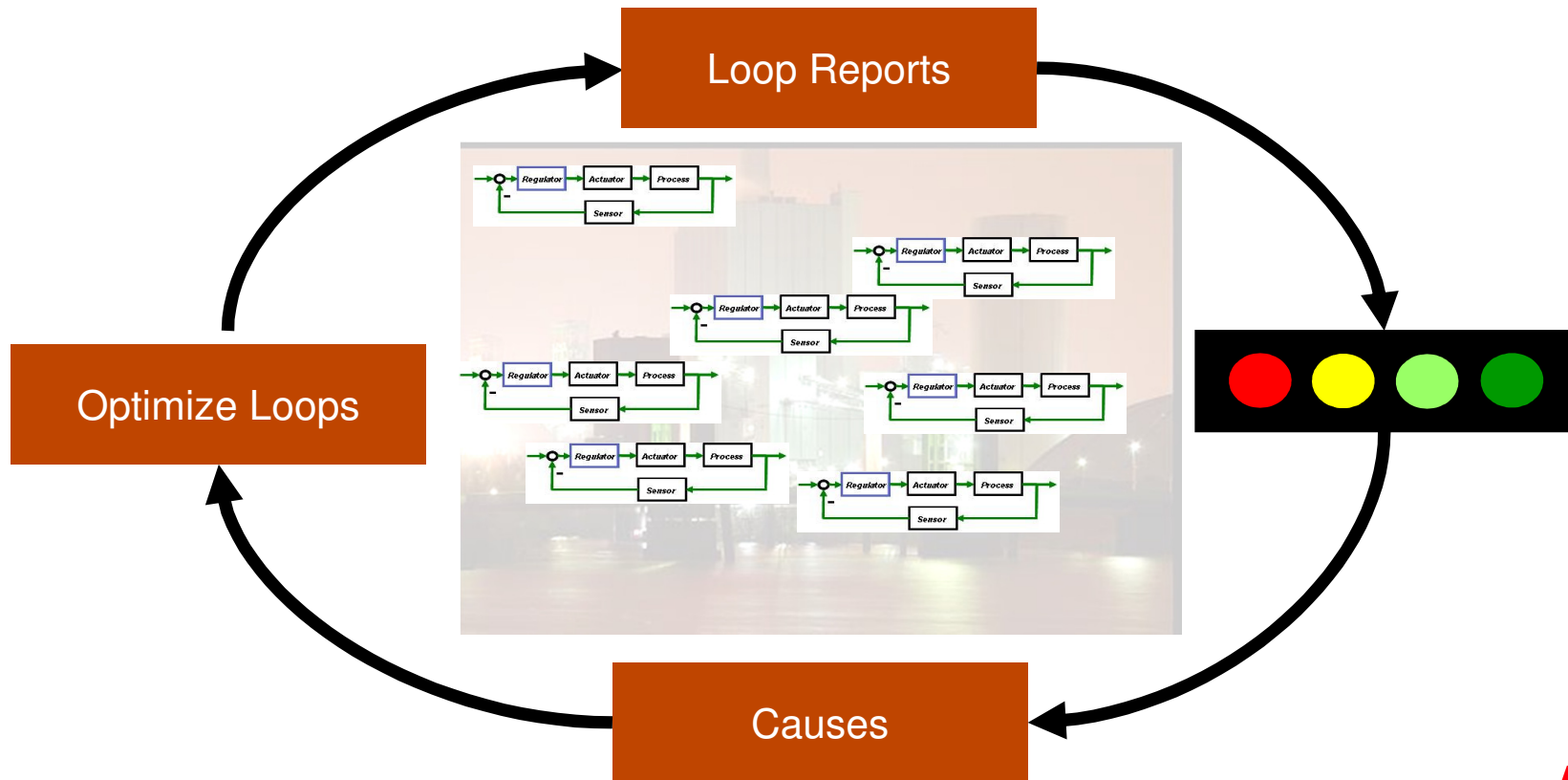
# Loop Auditing

- Transparent commissioning of control through loop optimizer.
- Model based tuning of each individual loop with a well documented report for each loop
- Reports are available at any time during commissioning giving a fast and accurate account of the loop commissioning status.
- Fully integrated into the System 800xA



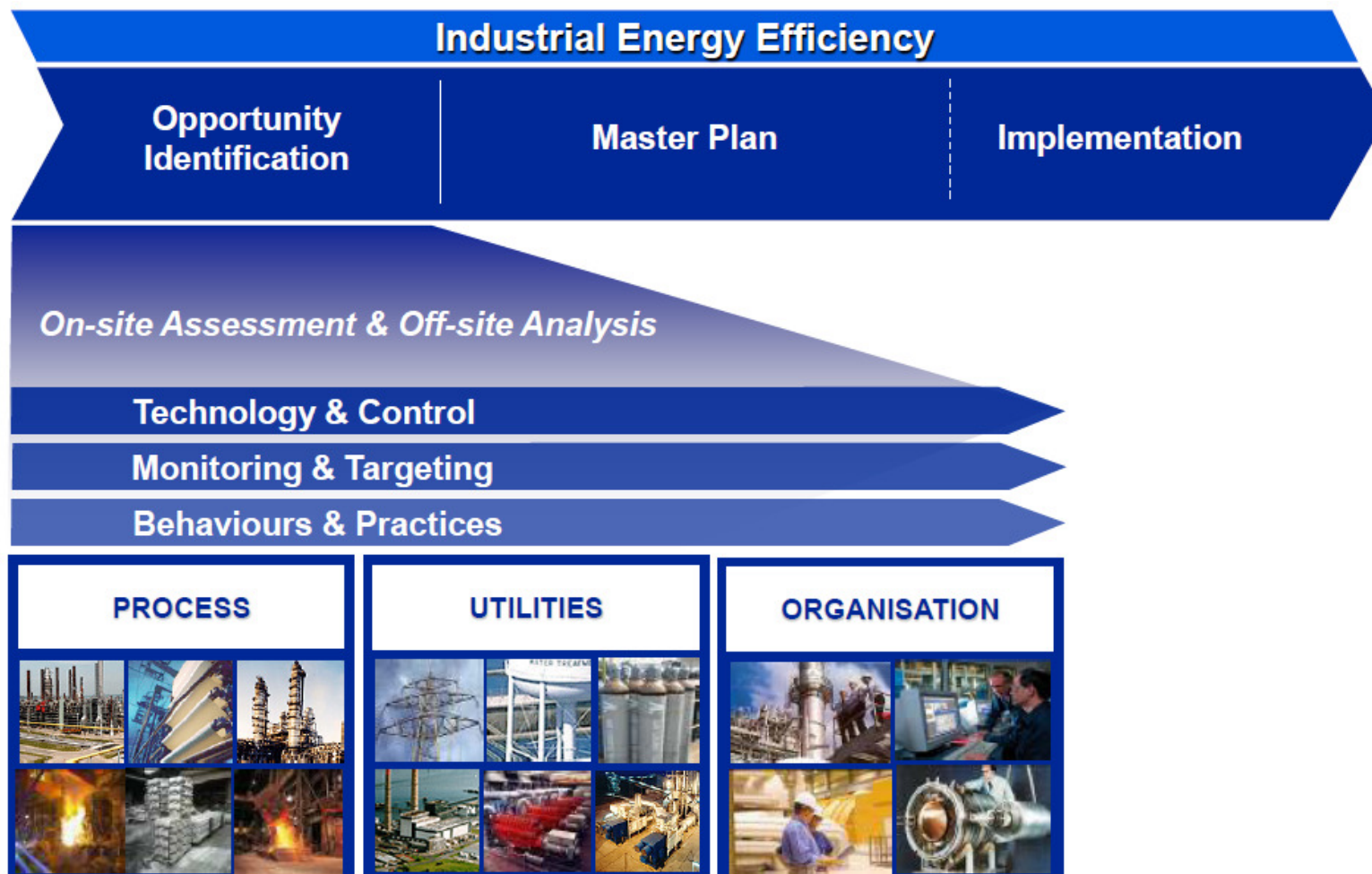
# Loop Auditing

- Loop auditing given feedback on current control loop performance to detect worsening control loop behavior.
- Indicating on possible causes for the worsening of the control loop performance.



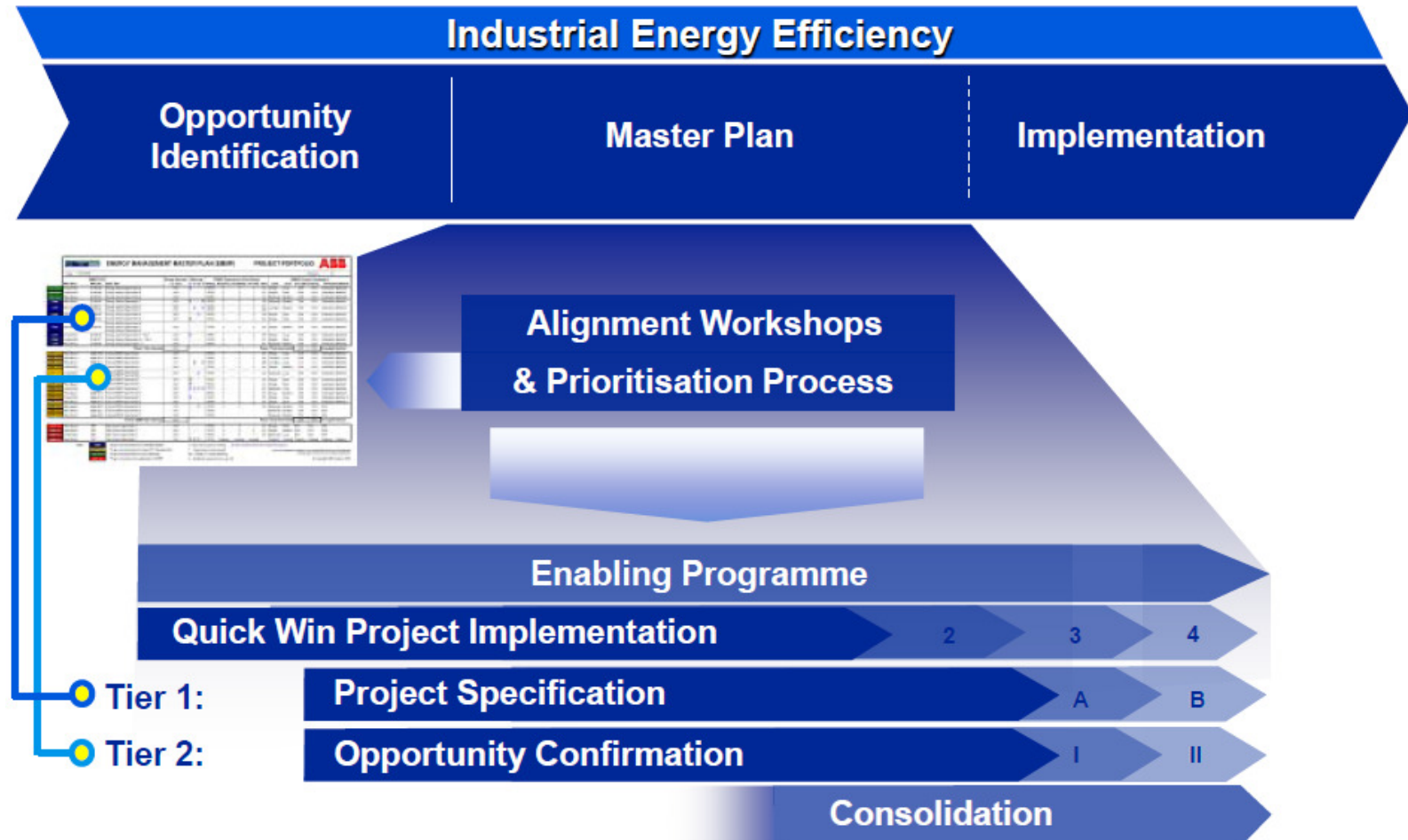
# Power and Water Plant Operations

## ABB Industrial Energy Efficiency (IEE) Assessment



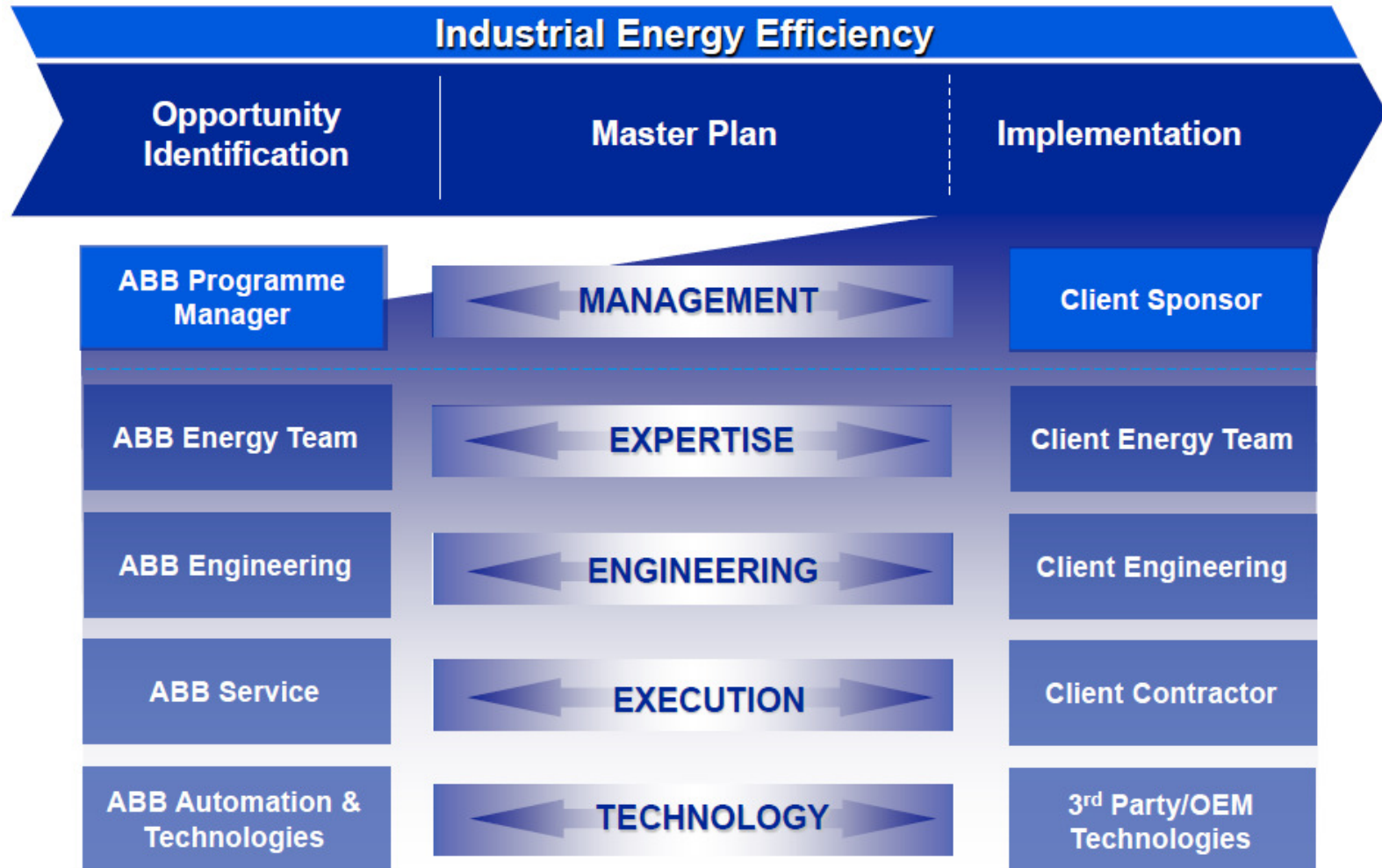
# Industrial Energy Efficiency (IEE)

## Master Plan



# Industrial Energy Efficiency (IEE)

## Implementation



Power and productivity  
for a better world™

