

Dual Flow Tray Technology

New Build Wet FGD System

- ▶ Superior Mass Transfer Capabilities allows comparable performance at reduced L/G ratios
- ▶ Design Comparison for 500 MW, 1.2% sulfur, 98% SO₂ removal

	Open Spray Tower	DFT Tower
Absorber Diameter, meters	15.0	15.0
Recycle Tank Retention Time, mins	5.0	5.0
Recycle Tank Height, meters	10.1	7.4
Number of Recycle Pumps	3+1	2+1
Recycle Pump Flowrate, m ³ /hr	6,100	6,670
Number of Trays	Zero (0)	One (1)
Overall Tower Height, meters	30.3	26.1
Absorber Power Consumption, kw	1,800	1,310
Pressure Drop, kPa	1.0	1.4

Dual Flow Tray Technology

New Build Wet FGD System

- ▶ Capital Cost Advantages for DFT Absorber vs Open Tower
 - ▶ Absorber is shorter in height
 - ▶ One (1) fewer recycle pump and piping system
 - ▶ Smaller absorber area footprint
 - ▶ Smaller absorber access structure
 - ▶ Thinner absorber shell steel
 - ▶ Reduced foundations
 - ▶ Less auxiliary piping
 - ▶ Less electrical cable and conduit
 - ▶ Less instrument and control cable
 - ▶ Lower construction costs

 - ▶ Identical (to slightly less) operating costs compared to open tower
 - ▶ Gas pressure drop power offset by lower recycle pumping rates
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Dual Flow Tray (DFT) Technology

New Build Wet FGD System

- ▶ Maintenance Advantage
 - ▶ Designed for Maintenance Loads
 - ▶ Initial construction staging platform
 - ▶ Installed inspection platform
 - ▶ Shorter outages
 - ▶ Minimal scaffolding and Lift Equipment reduce outage costs



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Existing Wet FGD Upgrades

- ▶ Performance Improvement Chemistry Options
 - ▶ Operating pH increase
 - ▶ Limited by chemistry concerns
 - ▶ Limestone stoichiometry
 - ▶ Sulfite to sulfate oxidation
 - ▶ Gypsum purity
 - ▶ Scaling
 - ▶ Higher Quality Limestone
 - ▶ Smaller grind
 - ▶ Higher Reactivity
 - ▶ Not typically reasonable option due to cost / availability

- ▶ Marginal performance improvement (1% - 3%)

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Existing Wet FGD Upgrades

- ▶ Performance Improvement by Equipment Modifications
 - ▶ Wall Rings
 - ▶ Reduces flue gas sneakage along side walls of absorber
 - ▶ Most effective only if spray distribution system is poorly designed
 - ▶ Marginal improvement expected (1% - 3%)
 - ▶ Higher Pressure Spray Nozzles
 - ▶ Smaller spray droplet / More surface area for mass transfer
 - ▶ Higher pumping power
 - ▶ Recycle Pump Motor change
 - ▶ Droplet coalescence limits improvement
 - ▶ Alternate Style Spray Nozzles
 - ▶ Smaller spray droplet / More surface area for mass transfer
 - ▶ Droplet coalescence limits improvement

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Existing Wet FGD Upgrades

► Performance Improvement by Equipment Modifications

► Additional L/G Ratio

- Generally required for significant efficiency improvement (>5%)
- Challenging to accomplish with an existing system
- Is there plot space available for larger or more recycle pumps?
- Is there absorber height available for more spray headers?
- Will the recycle pipe size need modification?
- Recycle tank retention time concerns
- Outage time requirement

► Dual Flow Tray Solution

- 1st upgrade in 1991 of four existing open spray towers in USA
- Most Recent upgrade done in May 2015 Startup
- 42 open spray / packed bed absorbers have been retrofitted with Dual Flow Trays
- Efficiency improvements from 80% up to 98%

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Existing Wet FGD Upgrades

► Dual Flow Tray Solution

- Ideal for performance improvement of an existing upflow open spray tower
- Full Scale Data indicate as much as 50% improvement in number of transfer units (NTU's) of existing open spray tower
 - 80% current SO₂ efficiency → 90% SO₂ efficiency
 - 85% current SO₂ efficiency → 93% SO₂ efficiency
 - 90% current SO₂ efficiency → 96% SO₂ efficiency
- 1.0 – 1.5 meters of space required between top of inlet flue gas duct and lowest spray level
- Adequate access into absorber recycle tank needed to install support steel and Tray Sections
- Adequate Fan Capacity for expected 0.4 kpa pressure drop increase



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